



Biological Wastewater Treatment Training Series Presentation #10: Aerobic Sludge Digestion

Larry W. Moore, Ph.D., P.E.,
WEF Fellow

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OUTLINE

- Sludge Treatment & Disposal Options
- Sludge Stabilization
- Process Fundamentals
- Aerobic Digestion Operating Conditions
- Use of Thickeners-Clarifiers
- ATAD Process
- Advantages & Disadvantages of Aerobic Digestion

Sludge Treatment & Disposal Options

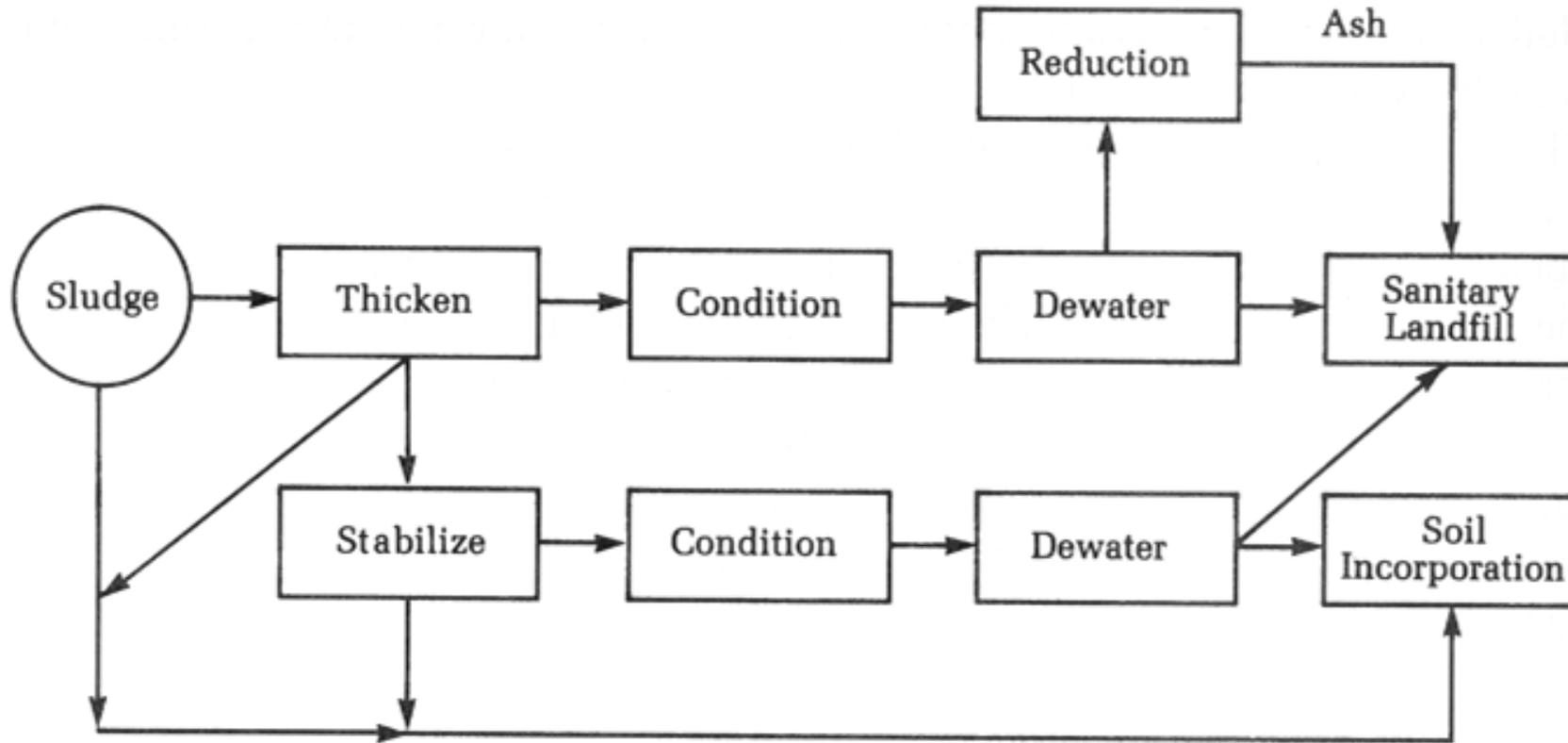


FIGURE 5-31
Basic sludge handling alternatives.

Ref: Davis, Cornwell, 1998, Intro to Environmental Engineering

Sludge Stabilization

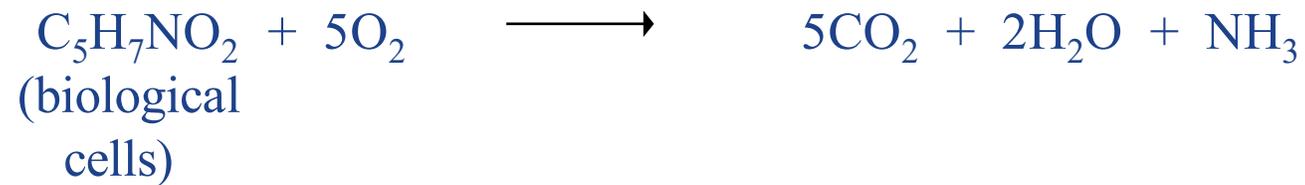
Why stabilize ?

- Reduce pathogen levels prior to final disposal
- Vector attraction reduction
- Increase the biostability of the sludge prior to final disposal

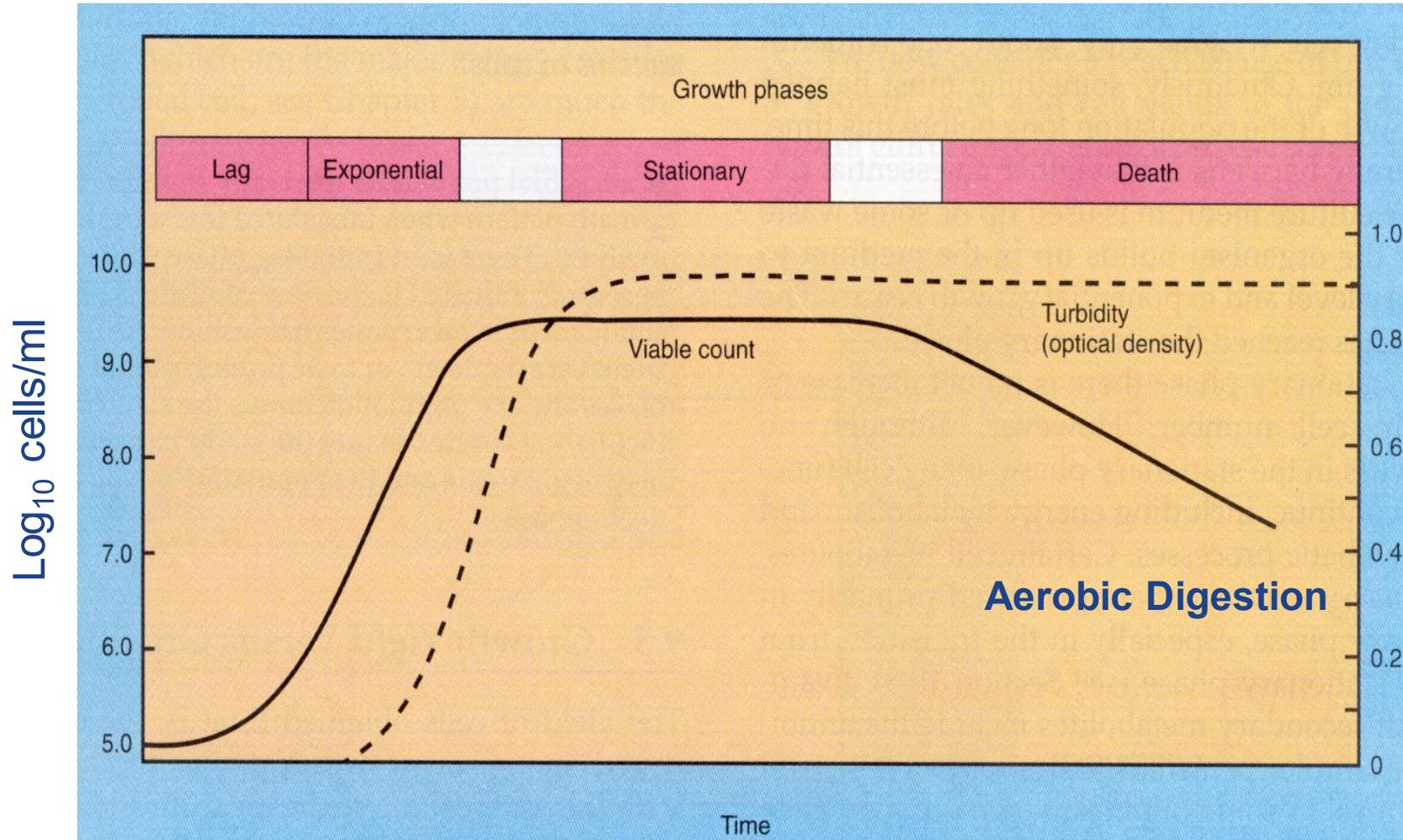
Processes for Stabilization

- **Aerobic Sludge Digestion**
- Anaerobic Sludge Digestion
- Lime Stabilization

Aerobic Digestion: Process Fundamentals

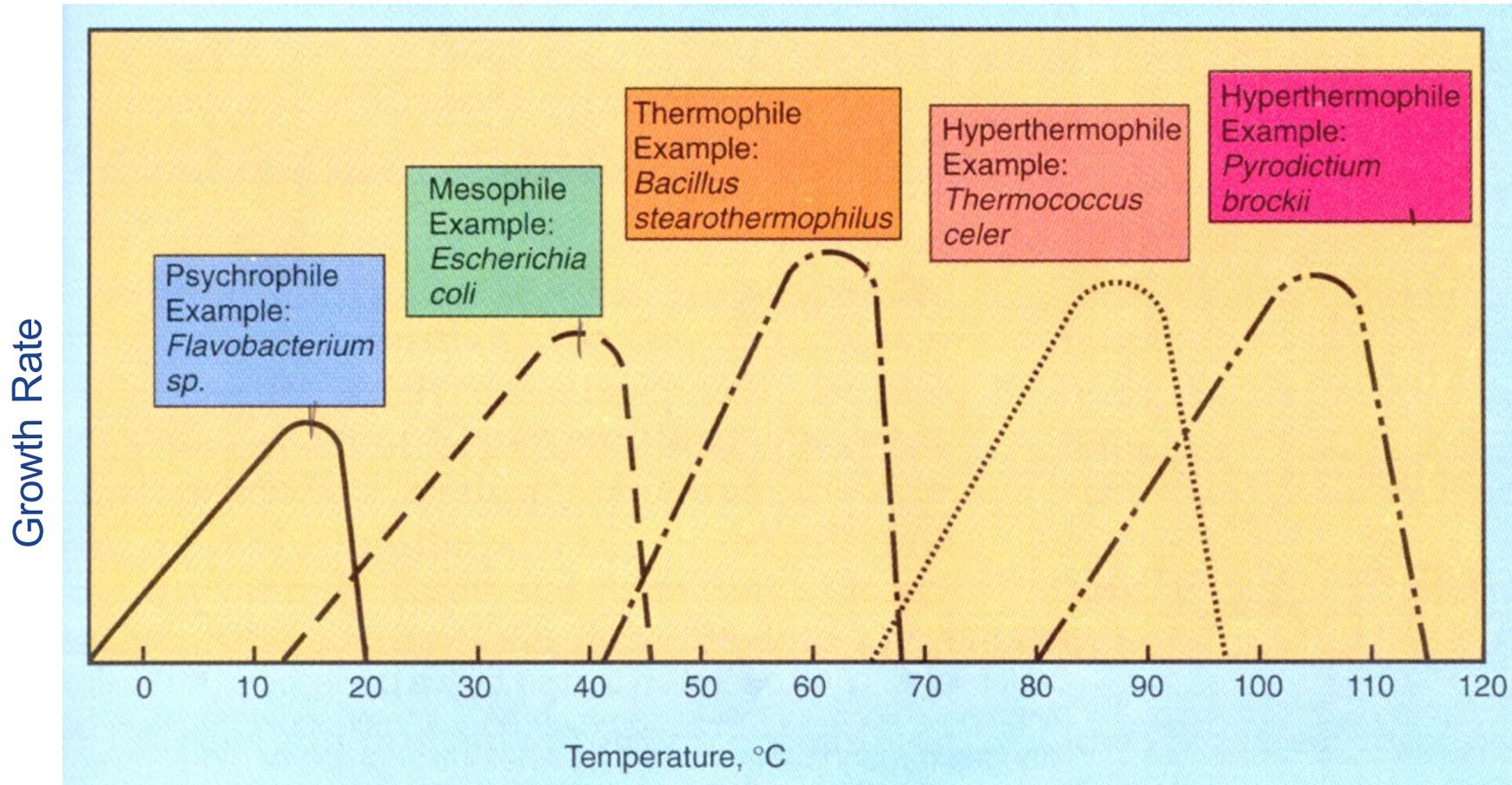


Microbial Growth Phases



Ref: Brock, Madigan, et al, Biology of Microorganisms

Temperature Classifications



Aerobic Sludge Digestion



Theoretical oxygen requirements = 2.0 lb O₂/lb biomass

Aerobic Digestion Design

- SRT at 20°C = 40 days; SRT at 15°C = 60 days (503)
- Volatile solids loading = 0.1 to 0.3 lb/(ft³-day)
- Oxygen requirements = 2.3 lb O₂/lb VSS destroyed
- Energy requirements for mixing = 100 to 200 hp/mil gal
- Dissolved oxygen residual = 1 to 2 mg/L
- Reduction of VSS = 38 to 50%

How You Operate Depends on...

- If treating sludge for direct land application
- If treating sludge for subsequent dewatering
- Types of dewatering equipment
 - Belt filter press
 - Centrifuge
 - Recessed plate pressure filter
 - Screw press
 - Sludge drying beds
- If pursuing Class A
- If you are hauling sludge away

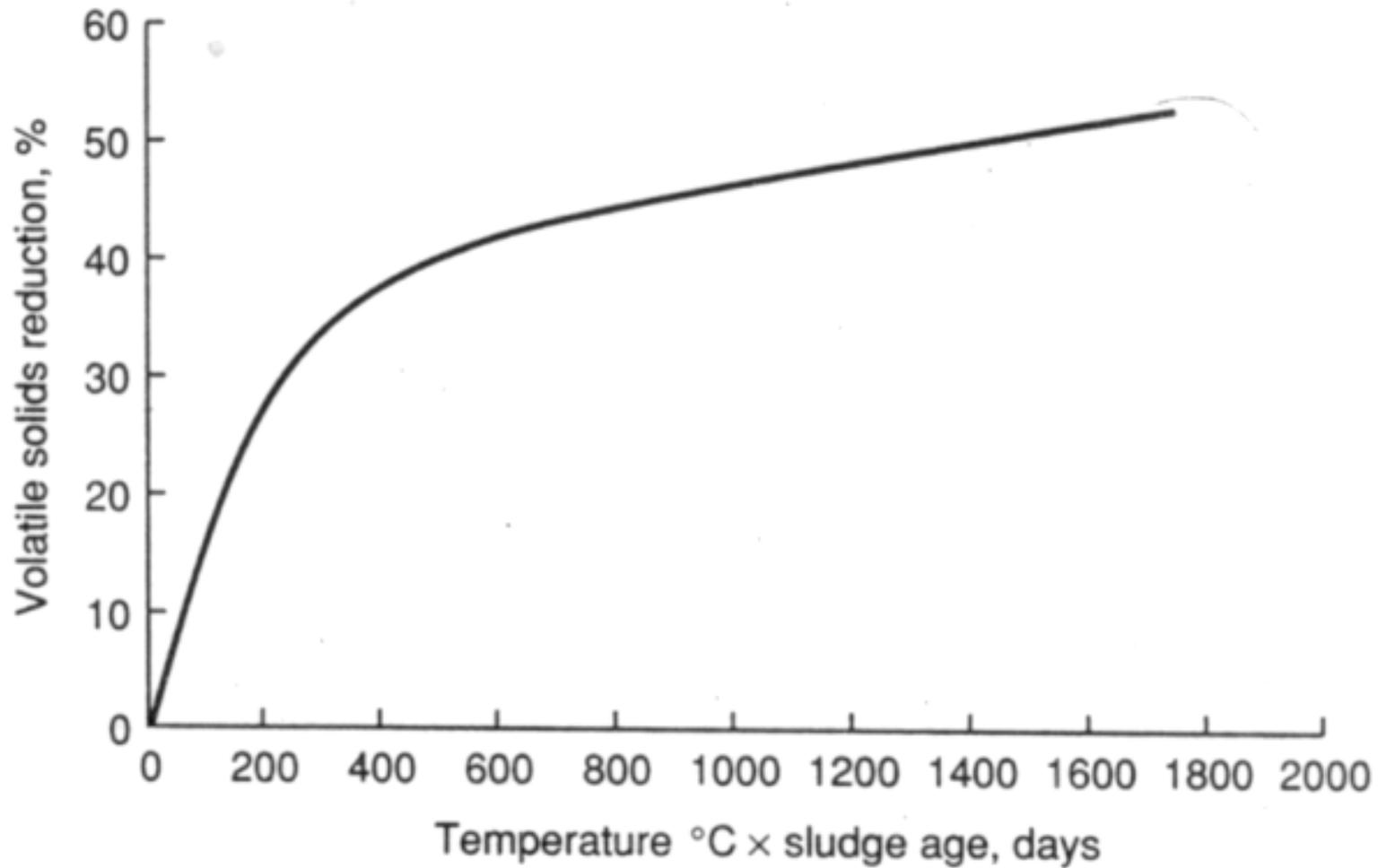
Other Factors to Consider

- Your influent sludge characteristics
 - % Total SS
 - % VSS
- Frequency of wasting
- If you are chemically treating influent or effluent
- Given digester design that you have:
 - Batch/continuous
 - Single or multi-tank & tank configuration/volume
 - Type of aeration
 - Amount of O₂ provided (e.g., blower size)
- Level of automation/instrumentation

To Meet 40 CFR 503

- Pathogen Reduction Alternatives (Class B):
 - MCRT of 60 days @ 15 C or 40 days @ 20°C
 - OR
 - Pathogen \leq 2,000,000 CFU or MPN per g TS
- Vector Attraction Reduction Alternatives:
 - VSS Reduction \geq 38%
 - OR
 - SOUR \leq 1.5 mg O₂ per hr per g TS @ 20°C

Aerobic Sludge Digestion



Aerobic Sludge Digestion: Scenario #1

- Activated sludge SRT = 10 days
- Desired VSS destruction in digester = 45%
- Design temperature = 20°C
- From previous figure, °C x days = 1100
- Required digester detention time = 55 days
- Oxygen requirements = 2.3 lb O₂/lb VSS destroyed

Aerobic Sludge Digestion: Scenario #2

- Activated sludge SRT = 40 days
- Desired VSS destruction in digester = 45%
- Design temperature = 20°C
- From previous figure, °C x days = 1100
- Required digester detention time = 55 days
- Empirically, only an additional 15 days of digestion time is needed; additional VSS destruction \approx 3%; oxygen requirements in digester are small.
- Reduce run time of digester aeration equipment

Estimated Aerobic Digester Supernatant Quality

Turbidity	120 NTU
Nitrate-N	40 mg/L
TKN	120 mg/L
COD	1,000 mg/L
PO ₄ -P	35 mg/L
BOD ₅	200 mg/L
TSS	400 mg/L
pH	5.7 to 8.0

Anoxic Operation

- Take advantage of anoxic operation, when possible
- But watch out for anaerobic conditions
 - Could lead to settling problems
 - Nocardia-like bulking

Volatile Solids Reduction Depends On:

- Nature of the sludge
- Hydraulic detention time
- Solids retention time (sludge age)
- Operating temperature

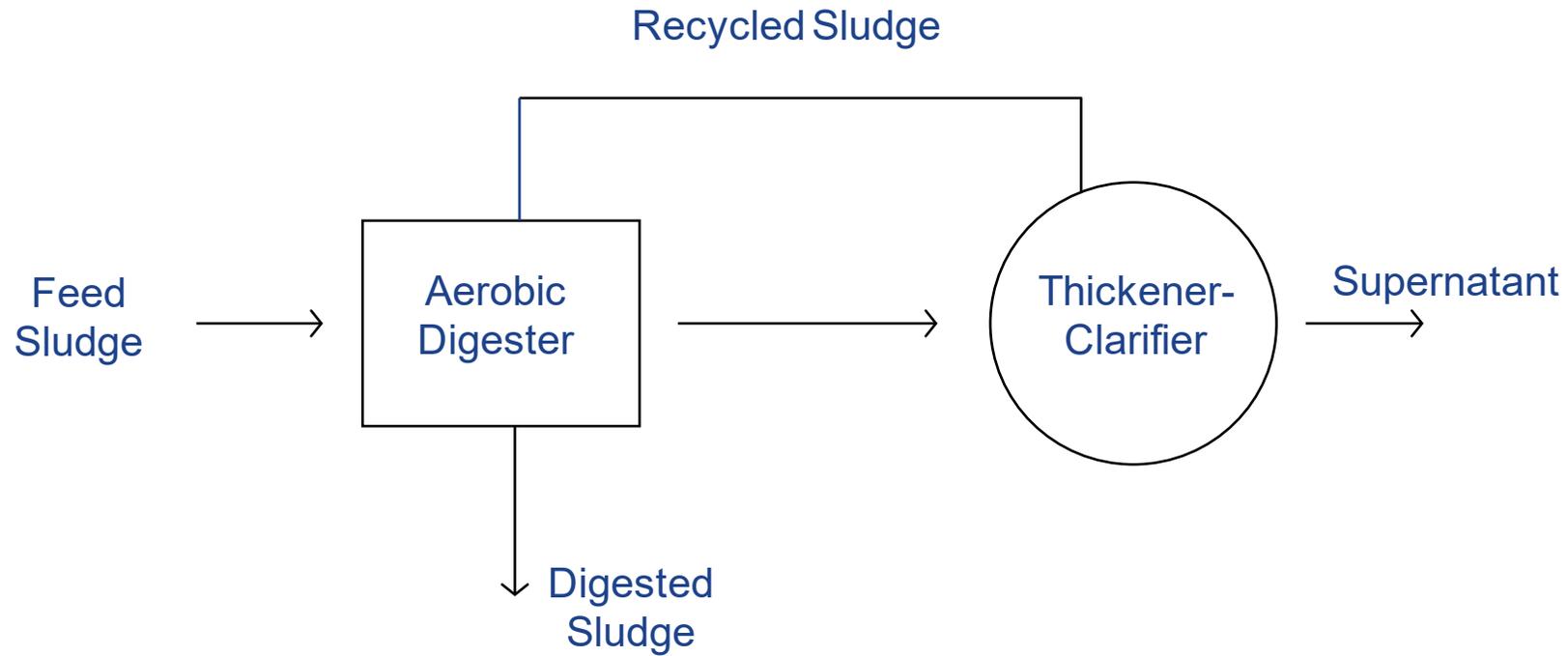
Mixing Requirements Depend On:

- Nature of the sludge
- Solids concentration
- Sludge temperature
- Tank depth

Use of Thickeners-Clarifiers

- Usually placed downstream of digester
- Should be designed for feed sludge plus recycled sludge flow
- Should have capacity to clarify the supernatant liquor and to thicken the settled sludge

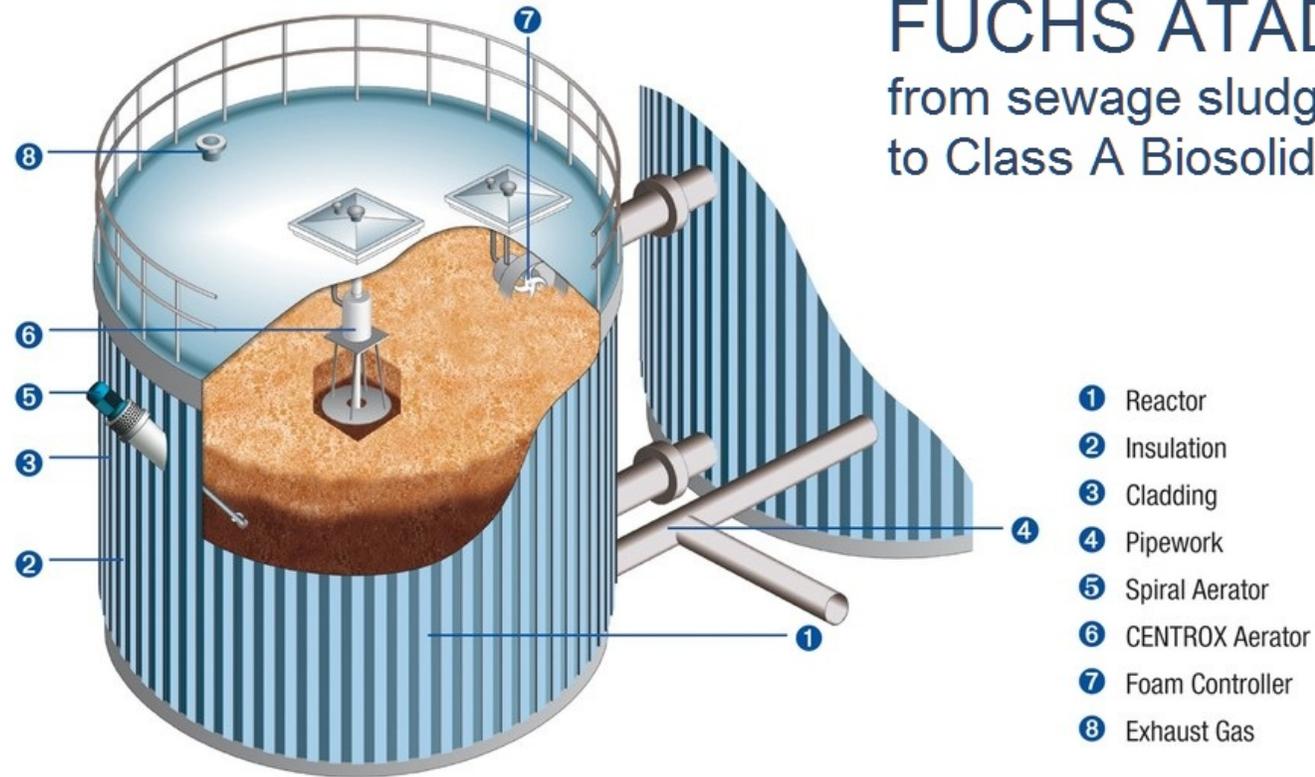
Aerobic Digester with Thickener-Clarifier



ATAD Process

- There is a more advanced aerobic digestion process called *Autothermal Thermophilic Aerobic Digestion*
- ATAD generally operates at 45-70+ °C (113-158+ °F) [i.e., sometimes beyond thermophilic range]
- Essentially pasteurization of sludge ... can produce Class A biosolids
- Two ATAD tanks in series typically are used
- External heating is not required because heat is generated by the oxidation of volatile solids and tanks are insulated

FUCHS ATAD System



FUCHS ATAD System



More on ATAD...

- Lower HRT & higher VSS reductions achievable
- Pathogens can be reduced to below detectable levels
- Robust process but way more complicated to design and operate
- Can achieve 40% VSS reduction in 4-8 days
- 440-640 kWh/Ton TS destroyed [ref: NORAM Bio Systems Inc, 2002]

Advantages of Aerobic Sludge Digestion

- Capital costs lower than anaerobic ($Q < 5$ mgd)
- Relatively easy to operate
- Does not generate nuisance odors (typically)
- Produces supernatant low in BOD, TSS, & $\text{NH}_3\text{-N}$ (typically)
- Reduces quantity of grease in the sludge mass
- Reduces pathogens to low levels

Other Advantages

- Can accept a wide range of waste types with less chance of toxicity (i.e., generally less sensitive to toxicants)
- No gas issue (safer than anaerobic digestion)
- No over-pressure concerns
- Relatively resistant to variations in loading, pH and metals interference

Disadvantages of Aerobic Sludge Digestion

- Can produce a digested sludge with poor dewatering characteristics
- Has high power costs to supply O₂
- Significantly influenced by temperature, location, and type of tank design
- Produces no usable by-product such as methane
- Possible odors if not operated properly

Potential Operating Problems

- Diffusers clogging
- Foaming
- Odors
- Insufficient pathogen control
- Grease buildup
- Digester return overflow
- Settling problems
- Aerator failure 😞

Thank you!

For Questions or Comments please reach out to the following:

Dr. Larry Moore
mlarry@bellsouth.net

Thomas Wenning
Oak Ridge National Lab
wenningtj@ornl.gov

