



### Welcome

- Welcome to the first Steam Virtual INPLT training series
- Eight, 2-1/2 hour webinars, focused on Industrial Steam Systems Energy Assessment and Optimization
- These webinars will help you gain a significant understanding of your industrial steam system, undertake an energy assessment using a systems approach, evaluate and quantify energy and cost-saving opportunities using US DOE tools and resources
- Thank you for your interest!







### **Steam Virtual INPLT Facilitator**



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### **Acknowledgments**

- Greg Harrell, PhD, PE
- US Department of Energy, Advanced Manufacturing Office
- Oak Ridge National Laboratory
- United Nations Industrial Development Organization
- Several industrial clients both in the US and internationally



# Agenda – Session ONE

- Welcome and Introductions
- Safety and Housekeeping
- Agenda for Steam Virtual INPLT (8 weeks)
- Today's Content:

#### **Industrial Steam Systems Fundamentals**

- Steam system components, thermodynamics
- Steam system overview

#### **Steam System Scoping Tool**

- Demonstration & Functionality
- Homework
- Kahoot Quiz Game
- Q&A











# Safety and Housekeeping

- Safety Moment
  - Steam can be extremely dangerous and extreme caution should be used while working with steam systems
  - Accidents can be life-threatening
- You are welcome to ask questions at any time during the webinar
- When you are not asking a question, please <u>MUTE</u> your mic and this will provide the best sound quality for all participants
- We will be recording all these webinars and by staying on-line and attending the meeting you are giving your consent to be recorded
  - A link to the recorded webinars will be provided, afterwards





# Steam Virtual INPLT Agenda

- Week 1 (April 6) Industrial Steam Systems Fundamentals and Introduction to SSST
- Week 2 (April 13) Focus on Steam System Generation and Introduction to DOE's MEASUR Tool
- Week 3 (April 20) Steam System Generation & Cogeneration (CHP)
- Week 4 (April 27) Steam System Distribution, End-Use & Condensate Recovery
- Week 5 (May 4) Energy Efficiency Opportunities in the Generation Area
- Week 6 (May 11) Energy Efficiency Opportunities in Cogeneration (CHP) Area
- Week 7 (May 18) Energy Efficiency Opportunities in Distribution, End-use and Condensate Recovery
- Week 8 (May 25) Industrial Steam System VINPLT Wrap-up Presentations





# Course Objectives

- Become familiar with US DOE tools and resources to assess, optimize and manage industrial steam systems
- Identify the measurements required to manage steam systems
- Measure boiler efficiency
- Estimate the magnitude of specific boiler losses
- Identify and prioritize areas of boiler efficiency improvement
- Recognize the impacts of fuel selection
- Characterize the impact of backpressure and condensing steam turbines





# Course Objectives

- Quantify the importance of managing steam consumption
- Identify the requirements of a steam trap management program
- Evaluate the effectiveness of thermal insulation
- Evaluate the impact of condensate recovery
- Recognize the economic impacts of steam system operations
- Use a systems approach to undertake a steam system energy assessment, identify opportunities and quantify the impacts
- Start thinking out-of-the-box and continue to reduce your plant's carbon footprint, reduce operating costs and enhance reliability

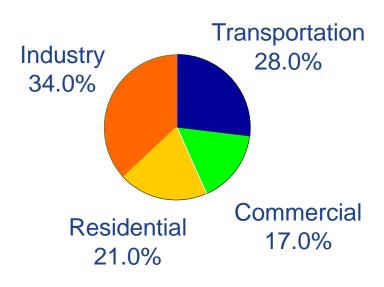




## Industrial Energy Overview

- Industry consumes 1/3 of U.S. energy
- More than 40% of U.S. natural gas is consumed by industry
- Approximately 28% of U.S. electricity demand is industrial
- Energy is key to economic growth and maintaining U.S. jobs in manufacturing

### 2004 Energy Use\*



\*Includes electricity losses

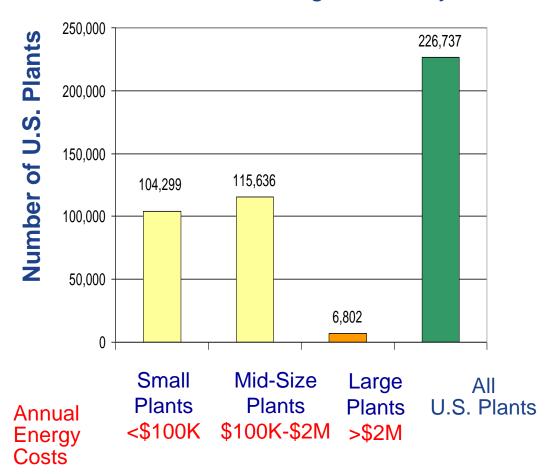
Source: DOE/EIA Monthly Energy Review 2004 (preliminary)



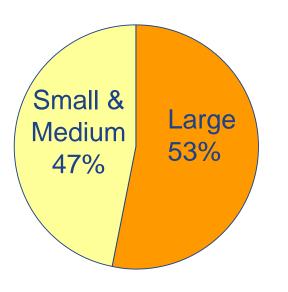


# Industrial Energy Consumption

U.S. Manufacturing Plants: By Size



Percent of Total Industrial Energy



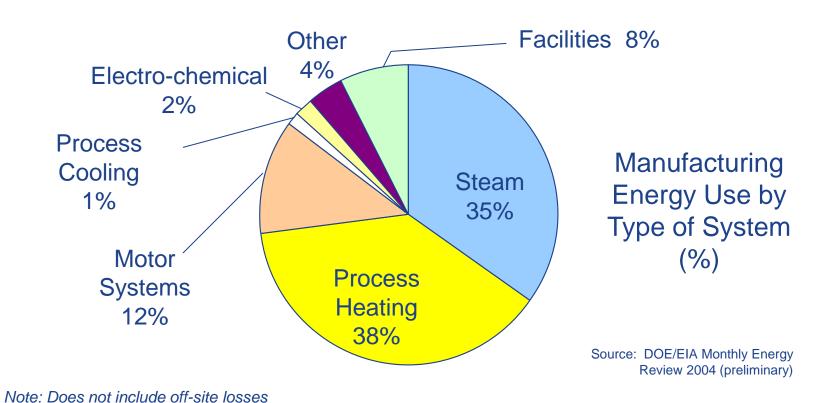
1998 EIA MECS





# Typical Industrial Energy Consumption

### Typical industrial facility energy consumption







### Industrial Steam Users

- Heavy Steam Users
  - Petroleum Refining
  - Forest Products (Pulp & Paper)
  - Petrochemicals
  - Inorganic chemicals
  - Large Food & Beverage
  - Rubber
  - Textiles
  - Pharmaceuticals
  - Manufacturing Assembly











### Industrial Steam Users

#### Medium Steam Users

- Breweries
- Bakeries
- Dairies
- Packaged Foods
- Metal Fabrication
- Large chiller systems

### Small Steam Users

- Electronics
- Paint booths
- Humidification systems









# Polling Question 1

- 1) Which industry do you belong to?
  - A. Heavy steam user Petrochemicals, Refineries, Forest Products, Chemicals
  - B. Heavy steam user Large Food and Beverage, Pharmaceuticals, Assembly, plants, etc.
  - C. Medium steam user Food, Fabrication, etc.
  - D. Small steam user Electronics, Specialty manufacturing, etc.
  - E. Not a steam user





# Polling Question 2

- 2) What is your major function in your current role at your plant?
  - A. Engineering (Design)
  - B. Operations & Maintenance (Engineering / Technical)
  - C. Operations & Maintenance (Management)
  - D. Plant management
  - E. Corporate-level management
  - F. Independent consultant / contractor
  - G. Other





## Why Use Steam?

- Extremely efficient as a heating source constant temperature, highest heat transfer (condensing) coefficients
- Extremely cost effective to distribute to point-of-use
- Can be controlled very accurately
- A very flexible energy transfer medium can be used for process heating as well as power generation
- Technology and applications are tried and proven at large as well as small-scale
- Significant system benefits!





**An Industrial Steam System** 



### Steam System Components

#### Generation

- Boiler
- Boiler auxiliaries
- Water treatment equipment
- Deaerator
- Feedwater Pumps
- Fuel storage and handling equipment
- Distribution
  - Steam piping
  - Pressure reducing stations

#### End-use

- Steam turbines
- Heat exchangers
- Live steam injection
- Stripping columns
- Evaporators, etc.

### Recovery

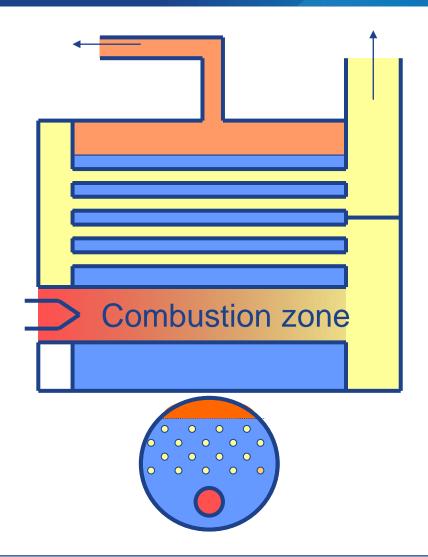
- Steam traps
- Condensate recovery and return system
- Condensate pumps





#### Fire-Tube Boiler

- Steam pressure limited
  - Typical 300 psig maximum
- Steam flow rate limited
  - Typical 1,200 BHp maximum
    - 40 klb/hr
- Saturated steam output
- One inherent efficiency advantage over water tube type – shell loss is minimal
- Generally manufactured offsite
- Many different styles

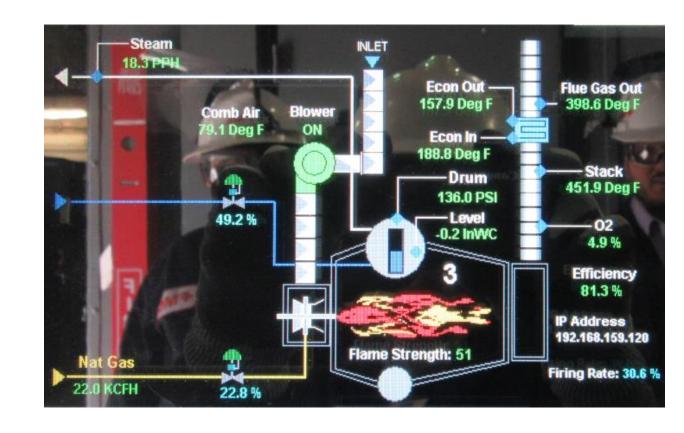






#### Water-Tube Boiler

- Operating pressures range from atmospheric to in excess of 3,000 psig
- Steam production ranges from 5,000 lb/hr to 10,000,000 lb/hr
- Saturated or superheated steam output
- Constructed onsite or offsite
- Many different styles
- Compact units now on the market!





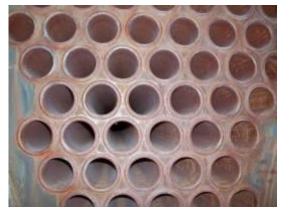


## Boilers

## Fire Tube Boiler









## Water Tube Boiler







### **Boiler Auxiliaries**

- Fans Air flow configuration
  - Forced draft
  - Induced draft
  - Balanced draft
- Combustion air preheaters
- Feedwater economizers / condensing economizers
- Fuel flow valves and combustion controls
- Excess air controls
- Sensors
- Soot blowers steam or compressed air
- Pollution control equipment





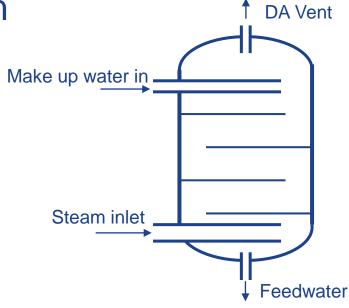






### Deaerator

- Removes dissolved oxygen from make-up water and condensate
- Boiler integrity
- Several different styles
  - Spray type
  - Tray type
- Maybe combined with feedwater heater and storage
- Will always have a steam vent!









## Pumps

- Boiler Feedwater (BFW)
- Condensate
- Make-up water
- Other auxiliary services











## Water Treatment Equipment

- Extremely important boiler water chemistry
- Integrity of boiler
- Depends on boiler pressure and water quality
- Several options
  - Softening
  - Dealkalization
  - Demineralization
  - Reverse osmosis
  - Condensate polishing
  - Chemical treatment











## Steam Piping

- Transports steam to end use
- Pipe racks
- Pressure headers
- Isolation valves
- Relief valves
- Drain points, etc













## Pressure Reducing Stations

- Also known as Letdown valves
- Provide steam flow control
- Provide pressure header balancing
- Operates on a feedback loop
- Always need a bypass for emergency and repair conditions







#### **Steam Turbines**

- Devices which convert thermal energy into shaft power
- Can generate electrical power through a generator
- Can drive a mechanical equipment – fan, pump, compressor, chiller, etc.
- Different types
  - Backpressure
  - Extraction
  - Condensing
  - Combination of the above









# Polling Question 3 and 4

- 3) Do you have steam turbines in your plant?
  - A. Back-pressure ONLY
  - B. Back-pressure and Condensing
  - C. Condensing ONLY
  - D. Do NOT have any steam turbines
  - E. Don't know
- 4) Do you have gas turbines in your plant?
  - A. Yes
  - B. No
  - C. Don't know





## Heat Exchangers

- Different types
  - Shell & Tube
  - Plate / Frame
  - Tube in tube
  - Spiral, etc.
- Based on applications
- Steam transfers thermal energy to process fluid and forms condensate
- Industry standards for designs and applications









## Other End Use Equipment

- Distillation tower
  - Stripping column
- Reboilers
- Reformers
- Separators
- Steam ejectors
- Steam injectors
- Thermocompressors



**Evaporators** 





# Other End Use Equipment

Cooker



**Feed Heater** 



Washing, Dyeing & Finishing





**Hot water heater** 





## Steam Traps

- Prevent steam from escaping without transfer of heat
- Several different types of traps
  - Thermostatic
  - Mechanical
  - Thermodynamic
  - Orifice
- Application very important
- Steam Trap Management













### Flash Tanks

- Recover flash steam from condensate
- Eliminate potential condensate return problems
  - Water hammer
  - Back-pressure
  - 2-phase flow
- Blowdown flash tanks reduce temperature of water before discharging to sewer









## Condensate Recovery System

- Primary / Secondary
- Pumped / Pressuredriven
- Pumped Electricdriven or Steam-driven
- Returns condensate back with the highest thermal energy to the boiler house









#### Condensate Tank

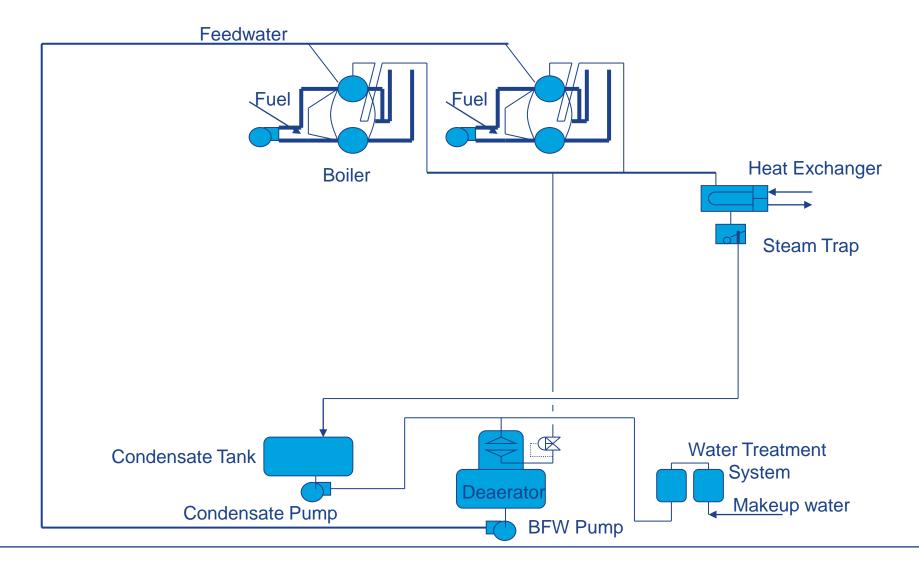
- Provides for a common receiver
- Typically, located above grade to provide for pump suction requirements
- May be combined with deaerator and feedwater heater and storage







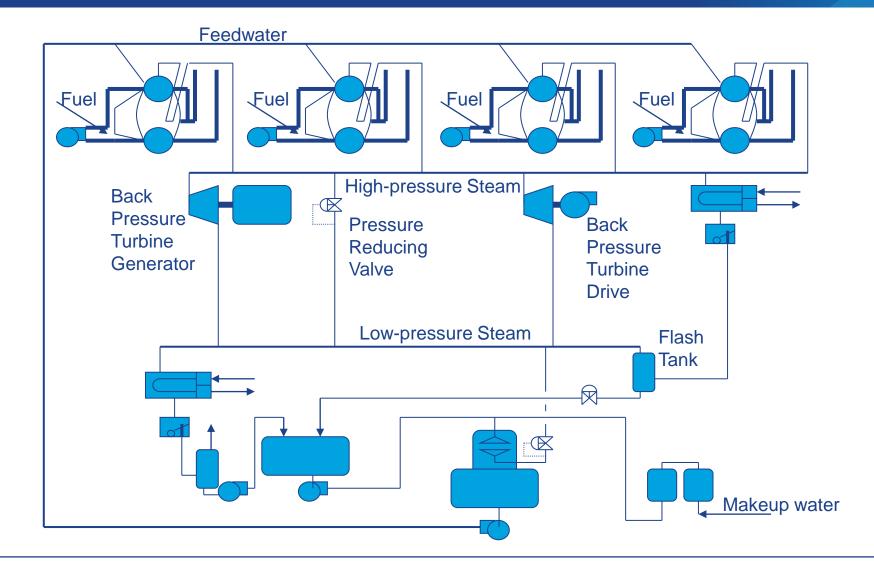
# One-Header Steam System







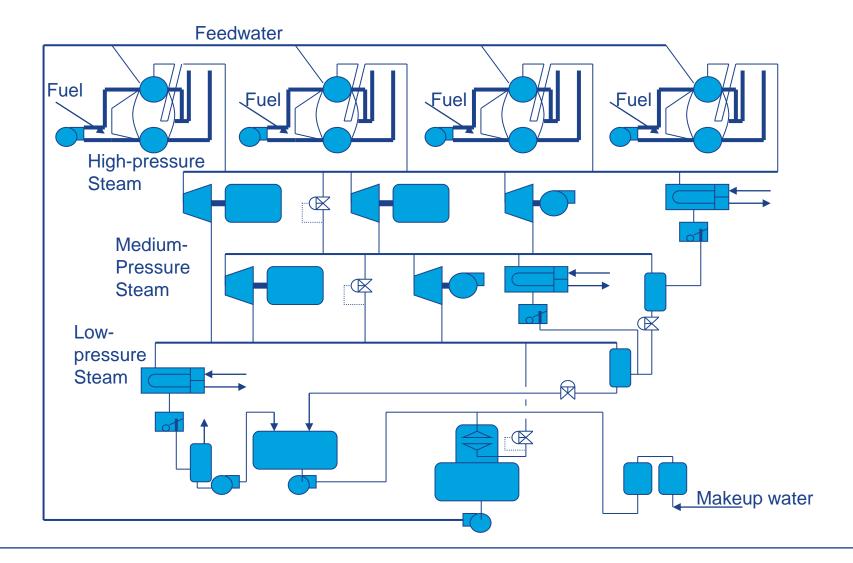
# Two-Header Steam System







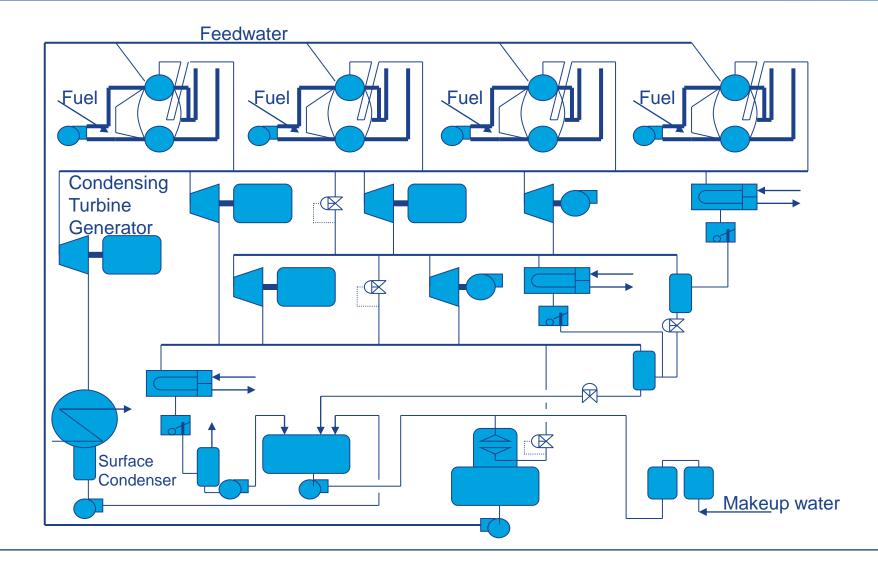
# Three-Header Steam System







# Three-Header Steam System







# Polling Question 5

- 5) What is the closest representation of the steam system in your plant?
  - A. One-header
  - B. Two-headers
  - C. Three-headers
  - D. Three-headers with steam turbines
  - E. Complex with more than Three-headers
  - F. Don't know
  - G. None of the above





# The Systems Approach

- Establish current system conditions, operating parameters, and system energy use
- Investigate how the total system presently operates
- Identify potential areas where system operation can be improved
- Analyze the impacts of potential improvements to the plant system
- Implement system improvements that meet plant operational and financial criteria
- Continue to monitor overall system performance





#### Tools

- In order to properly evaluate steam systems, the physics of each process must be understood
  - Thermodynamics
  - Heat transfer
  - Fluid flow
- US DOE Tools
  - Steam System Survey Guide
  - Steam System Scoping Tool (SSST)
  - MEASUR Steam System
  - Insulation Evaluation Software 3E Plus
- Process measurements





**Steam System Thermodynamics** 



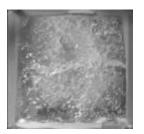
#### Steam Thermodynamics

- Thermodynamic States of a Pure Substance
  - Subcooled
    - Liquid (Water)
    - Temperature and Pressure are independent
    - Energy content ∞ Temperature



- Liquid / 2-Phase / Vapor
- Temperature and Pressure are dependent
- 0 ≤ Quality ≤ 1
- Superheated
  - Vapor (Steam)
  - Temperature and Pressure are independent
  - Energy content ∞ Temperature & Pressure











# Steam Thermodynamics

- Steam Properties
  - MEASUR
  - Steam Tables
    - Mollier Diagrams
  - ASHRAE Fundamentals Handbook
    - Tabulated Data
    - P-h diagram
  - Software Programs
    - Equation of State for different refrigerants
    - Engineering Equation Solver (EES)
    - Other
  - National Institute of Standards & Testing (NIST)
- Reference Point
  - Maybe different for different sources!!





#### Steam System Analysis

- Steady State Steady Flow (SSSF) analysis
  - Neglect the time dependent terms
  - Dynamic responses are not considered
  - Start-up, Shut-down and upset (or trip) conditions are neglected
- Average operating conditions are used
- Seasonality, Production rates can be dealt with "bin analysis" methodology
- IMPACT level-analysis is conducted on systems





#### Conservation of Mass

- Law: Mass is neither created nor destroyed in the control volume
- Mathematically,
  - Mass flow in = Mass flow out
- Equation format
  - $\Sigma M_{in} = \Sigma M_{out}$

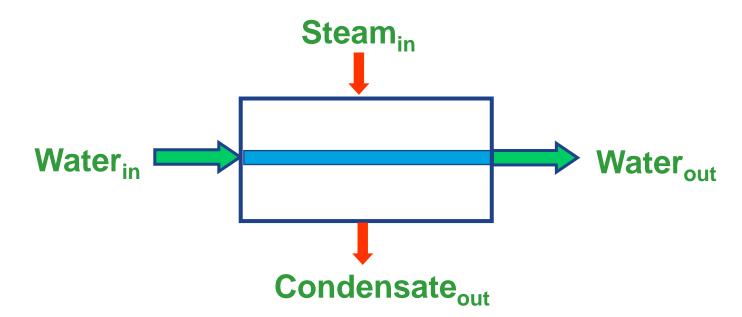


State of substance & Volume flow can change





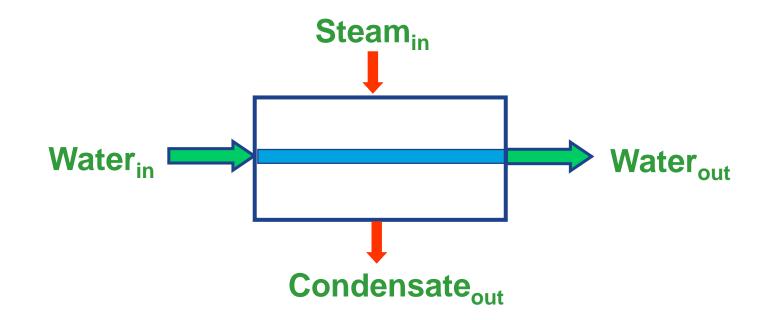
- A shell and tube heat exchanger is used to heat water using steam
- Water flow rate measured as 100 gpm
- Steam flow rate is not known







- Apply Steady State Steady Flow Conservation of Mass
- Water side: Water flow in = Water flow out
- Steam side: Steam flow in = Condensate flow out







Apply Steady State Steady Flow – Conservation of Mass

- Water side:
  - Water flow in = 100 gpm = 50,000 lb/hr
  - Water flow out = 100 gpm = 50,000 lb/hr

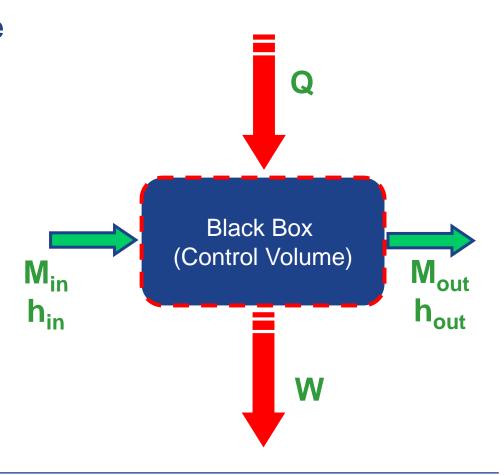
Steam side: Steam flow in = Condensate flow out





#### Conservation of Energy

- Law: Energy can neither be created nor destroyed in the control volume. It can only be changed from one form to another.
- Mathematically,
  - Energy flow in + Heat = Energy flow out + Work
- Equation format
  - $\Sigma M_{in}^* h_{in} + Q = \Sigma M_{out}^* h_{out} + W$
  - h specific enthalpy (Btu/lb)





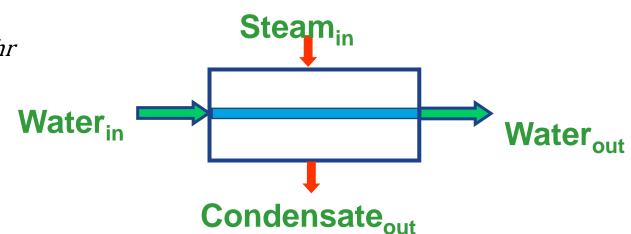


- Water inlet temperature = 65°F
- Water outlet temperature = 135°F
- Specific heat of water = 1.0 Btu/lb°F
- Heat transferred to water =  $M_{water} * C_p * (T_{out} T_{in})$

$$Q = 50,000 \times 1.0 \times (135 - 65) \; Btu/hr$$

$$Q = 3,500,000 \; Btu/hr$$

$$Q = 3.50 \, MMBtu/hr$$







- Steam inlet conditions: Saturated steam at atmospheric pressure (0.0 psig)
- Condensate outlet conditions: Saturated at T = 212°F
- Heat transferred by steam =
   M<sub>steam</sub> \* h<sub>steam</sub> M<sub>condensate</sub> \* h<sub>condensate</sub>
- No shaft work is done in the control volume: W = 0
- Heat transferred to water = Heat transferred from steam
- Conservation of Mass: M<sub>steam</sub> = M<sub>condensate</sub>





- $Q = M_{steam} * (h_{steam} h_{condensate})$
- Steam Property tables provide information on steam and condensate enthalpies
- h<sub>steam</sub> Saturated steam at 0.0 psig = 1,150 Btu/lb
- h<sub>condensate</sub> Saturated condensate at 212°F = 180 Btu/lb

$$Q = M_{steam} \times (1,150 - 180)$$

$$3,500,000 = M_{steam} \times (970)$$

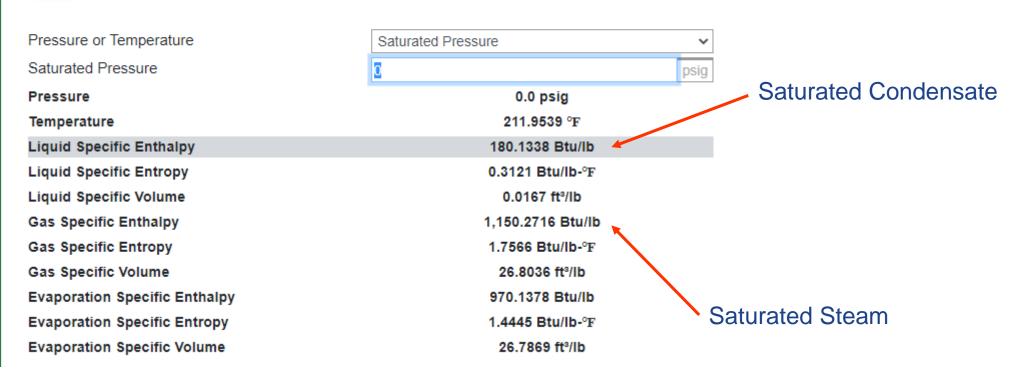
$$M_{steam} = 3,608 \frac{lb}{hr} = 3.61 \frac{klb}{hr}$$





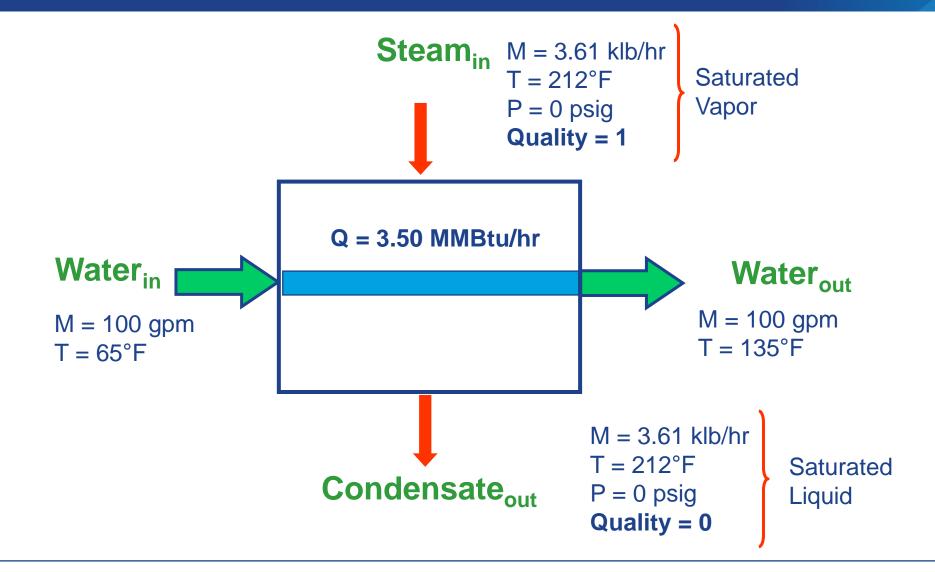


#### SATURATED PROPERTIES







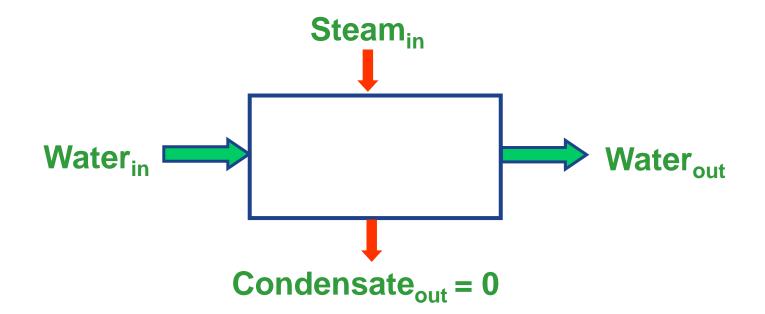






#### Example: F2 (Food for thought!)

- Steam is directly injected in a vessel to heat water
- Water flow rate required (& measured) by process is 100 gpm
- Steam flow rate is unknown







# Fuel Heating Value

- The energy content of a fuel is determined by a combustion process
  - The combustion process begins and ends at ambient temperature
    - Constant pressure analysis provides the most accurate heating value
  - The energy released during the combustion process is measured
    - The energy released is the Heat of Combustion for the fuel
      - This is also the *calorific value*, the *Btu value*, and the *heating value*
- Fuels containing hydrogen will form water during combustion

$$CH_4+2O_2 \rightarrow CO_2+2H_2O$$
 +Energy Release





# Higher Heating Value

- Water (H<sub>2</sub>O) formed during the combustion process is initially steam but condenses during the heating value test
  - Each pound of water releases approximately 1,000 Btu of energy by condensing
    - This energy release is measured in the <u>Higher Heating Value</u>
- In the United States Higher Heating Value is the most common convention
  - The primary exception is the combustion turbine arena

$$CH_4 + 2O_2 \rightarrow CO_2 + 2H_2O + \text{Energy Release}$$





### Lower Heating Value

- The Lower Heating Value is the energy liberated from a combustion process with no latent energy release from condensation
- The Lower Heating Value is generally determined by calculation from the higher heating value and the fuel composition
- In most boiler operations the flue gas will exit the boiler with no condensate
- The Lower Heating Value is the convention in most of the world

$$CH_4 + 2O_2 \rightarrow CO_2 + 2H_2O$$
 + Energy Release





# Higher and Lower Heating Value

- The numeric difference between the higher and lower heating values depends on the hydrogen content of the fuel
  - Natural gas difference is 10%
  - Fuel oil difference is 6%
  - Coal difference is ~4%
  - Green wood difference can be more than 20%
- In the United States most fuels are marketed based on the fuel higher heating value
- The primary point of concern is consistency





# Polling Question 6

- 6) What fuels are used in your plant to generate steam (Select all that apply)?
  - A. Natural gas
  - B. #2 Oil
  - C. #6 Oil
  - D. Coal
  - E. Wood
  - F. Biomass, Biogas, etc.
  - G. Other
  - H. Don't know
  - I. I don't generate Steam





#### **Conduction Heat Transfer**

$$\dot{Q}_{conduction} = -k A \frac{\delta T}{\delta x}$$

$$\dot{Q}_{\text{radial}} = \frac{-k \ 2 \ \pi \ L(T_2 - T_1)}{\ln\left(\frac{R_2}{R_1}\right)}$$

$$\dot{Q}_{\text{constantarea}} = -k A \left( \frac{T_2 - T_1}{\chi_2 - \chi_1} \right)$$

$$k = thermal\ conductivity\ [=]\ \frac{Btu}{hr\ ft\ °F}$$





#### **Convection Heat Transfer**

$$\dot{Q}_{convection} = h A \Delta T$$

$$h = 0.1 \frac{Btu}{hr ft^2 \circ F}$$
 to  $1,000 \frac{Btu}{hr ft^2 \circ F}$ 





#### Radiation Heat Transfer

$$\dot{Q}_{radiation} = \gamma \sigma \varepsilon A \left( T_1^4 - T_2^4 \right)$$

$$\gamma = view \ factor = 0.0 \ to \ 1.0$$

$$\sigma = \text{Stephan} - \text{Boltzmann}$$
 Constant =  $0.1714 \left(10^{-8}\right) \frac{Btu}{hr \ ft^2 \circ R^4}$ 

$$\varepsilon = emissivity = 0.0 to 1.0$$





# Key Points / Action Items



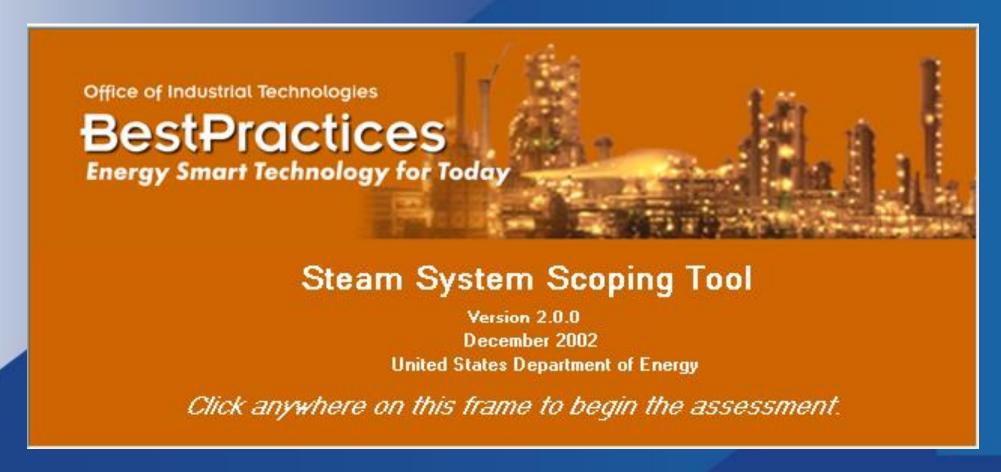
- 1. Use a Systems Approach to optimize steam systems
- 2. There are four major areas of a steam system Generation, Distribution, End-Use & Recovery
- 3. An understanding of the laws of thermodynamics, heat transfer, fluid flow and steam properties is required for a steam system analysis
- 4. Steam is used all across industry to do various tasks and is the most effective medium to transport energy and produce shaft work (or power)







# Steam System Scoping Tool – (SSST)





### Steam System Scoping Tool - SSST

- SSST is a software-based questionnaire designed to enhance awareness of areas of steam system management
- Divided into typical steam system focus areas
- Provides the user a score that is indicative of management intensity and serves as a guide to useful information
- Tool to identify potential improvement opportunity areas
- Will NOT quantify the energy savings opportunities





#### **Intended SSST Users**

- Industrial manufacturers
  - Plant managers
  - Utility managers
  - Plant process engineers
- Energy experts/consultants for assessment
- Can also be used by institutional, commercial steam users





# **SSST Organization**

- Introduction
- Steam system basic data
- Steam system profiling
- Overall system operating practices
- Boiler plant operating practices
- Distribution, end use and recovery operating practices
- Summary results
- Next steps





# Obtaining Data for SSST Input

- Sources of data:
  - Actual current measurements
  - Computerized or print copy historical records
  - Information on procedures from:
    - Plant engineer/utilities/maintenance manager(s)
    - Boiler operator
- Full Completion:
  - 26 questions expected time: 45 min (max)





## **Steps for Use of SSST**

- Open SSST
- Review SSST sections to identify needed input data
- Obtain input data
- Optionally complete steam system basic data section
- Insert answer choices into SSST sections





## Steps for Use of SSST (Continued)

- On summary results screen note scores achieved in major tool sections
- Compare scores achieved with those for similar plants
- Identify and prioritize steam system improvement opportunities
- Utilize resources identified in "next steps" section for assistance in implementing steam system improvements





## **Interpreting Summary Results**

- Average score (65%) reported based on results collected from several industrial steam plants:
  - Steam system profiling: 63%
  - Steam system operating practices: 69%
  - Boiler plant operating practices: 63%
  - Distribution, End-Use, Recovery: 58%
- Your scores will vary!
- Excellent place to start understanding the steam system and its operations including management practices





# Next Steps Directed by SSST

- Focus on areas requiring attention
- Investigate resources
  - Consult the U.S. DOE Web site
    - http://energy.gov/eere/amo/advanced-manufacturing-office
  - Steam System Survey Guide
  - U.S.DOE Steam Tip Sheets
  - Improving Steam System Performance: A Sourcebook for Industry
- Use US DOE's MEASUR
  - Calculators
  - Steam Assessment
- Use the Insulation Tool (3E Plus)





#### Common BestPractices - Generation

- Minimize excess air
- Install heat recovery equipment
- Clean boiler heat transfer surfaces
- Improve water treatment to reduce boiler blowdown
- Recover energy from boiler blowdown
- Add/restore boiler refractory
- Minimize the number of operating boilers
- Optimize deaerator vent rate





#### Common BestPractices - Distribution

- Repair steam leaks
- Minimize vented steam
- Ensure that steam system piping, valves, fittings and vessels are well insulated
- Isolate steam from unused lines
- Minimize flows through pressure reducing stations
- Reduce pressure drop in headers
- Drain condensate from steam headers





#### Common BestPractices – End-Use

- Reduce steam usage by a process
  - Improving the efficiency of the process
  - Shifting steam demand to a waste heat source
- Reduce the steam pressure needed by process, especially in cogeneration systems
- Upgrade low pressure (or waste) steam to supply process demands
- Process integration leading to overall energy optimization of the plant





### Common BestPractices - Recovery

- Implement an effective steam-trap management and maintenance program
- Recover as much as possible of available condensate
- Recover condensate at the highest possible thermal energy
- Flash high-pressure condensate to make low-pressure steam





## Key Points / Action Items



- 1. Use a systematic approach (gap analysis, comparison to BestPractices) to identify potential energy saving opportunities that may exist in steam systems
- 2. Use the Steam System Scoping Tool (SSST) to provide a high-level overview of operational, maintenance and management BestPractices
- 3. Once gaps are identified, delve into more detail using the other US DOE's tools and resources
- 4. Quantify, prioritize, implement and continue to monitor

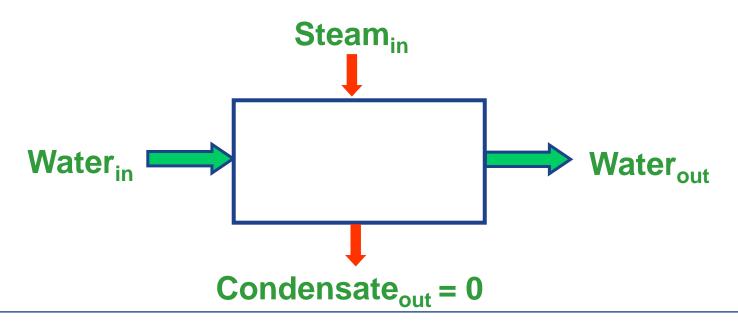






#### Homework #1

- Steam is directly injected in a vessel to heat water from 65°F to 135°F and the required flow for the process need is 100 gpm.
  - Calculate the steam flow rate required
  - Compare the results with the indirect heat exchange application and comment on which method would you recommend for use in your plant.







#### Homework #1

 Use the Steam System Scoping Tool (SSST) on your industrial plant steam system and prepare a high-level list of potential areas for investigation in a steam system energy assessment over the next 6 weeks.

 Prepare a line diagram for your steam system showing the boilers, headers, major end-users and condensate return system.
 Indicate pressures, steam flows and anything important for your system.





Thank You all for attending today's webinar.

See you all on next Tuesday – April 13, 2021 – 10 am ET

If you have specific questions, please stay online and we will try and answer them.

Alternately, you can email questions to me at rapapar@c2asustainable.com

